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⑧ Catalytic process for manufacture of low pour point lubricating oils.

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Description

This invention relates to a process for manufacture of low pour point lubricating oils, in particular to a specific process for the manufacture of dewaxing hydrocracked oils.

5 The desirability of upgrading a crude fraction normally considered unsuitable for lubricant manufacture to one from which good yields of lubricating oil can be obtained has long been recognised. The so-called "hydrocracking process", sometimes referred to in the art as "severe hydrotreating", has been proposed to accomplish such upgrading. In this process, a suitable fraction of a poor grade crude, such as a California crude, is catalytically reacted with hydrogen under pressure. The process is complex in
10 that some of the oil is reduced in molecular weight and made unsuitable for lubricating oils, but concurrently, a substantial fraction of the polynuclear aromatics is hydrogenated to form naphthenes and paraffins. Process conditions and choice of catalyst are selected to provide an optimal conversion of the polynuclear aromatic content of the stock since this component degrades the viscosity index and stability of the stock. Also, in the hydrocracking process, paraffins can be isomerized, imparting good viscosity
15 index characteristics to the final lubricating oil product. For purposes of this invention, the term "hydrocracking" will be employed for the foregoing process step and to distinguish this step from the "hydrotreating" step to be described below, the purpose of the latter being to stabilize the lubricating oil base stock produced by hydrocracking. For purposes of this invention, the hydrocracking and hydrotreating steps may be distinguished also by the amount of hydrogen consumed, the hydrocracking step typically
20 consuming about 178—356 l/l (1000—2000 SCF/bbl) (standard cubic feet per barrel of feed) while the hydrotreating step consumes only about 17.8—35.6 l/l (100—200 SCF/bbl).

The hydrocracking process for increasing the availability of lubricating oils has an attractive feature that is not immediately apparent. Generally, the composition and properties of hydrocracked stocks are not particularly affected by the source and nature of the crude, i.e. they tend to be much more alike than lubricating oil fractions prepared from different crudes by conventional means. Thus, the process promises to free the refiner from dependence on a particular crude, with all of the advantages that this freedom implies.

Hydrocracked lubricating oils, however, in general have an unacceptably high pour point and require dewaxing. Solvent dewaxing is a well-known and effective process but expensive. More recently, catalytic methods for dewaxing have been proposed. U.S. Reissue Patent 28,398 describes a catalytic dewaxing process wherein a particular crystalline zeolite is used. To obtain lubricants and speciality oils with outstanding resistance to oxidation, it is often necessary to hydrotreat the oil after catalytic dewaxing as illustrated by U.S. Patent No. 4,137,148. U.S. Patent Nos. 4,283,271 and 4,283,272 teach continuous processes for producing dewaxed lubricating oil base stock including hydrocracking a hydrocarbon feedstock, catalytically dewaxing the hydrocracked oil and hydrotreating the dewaxed hydrocracked oil. Both latter patents, recognised as advances in the art, teach use of catalyst comprising zeolite ZSM-5 or ZSM-11 for the dewaxing phase.

In our copending European patent application 82300226.6 we have disclosed a process for catalytically dewaxing a hydrocarbon oil that contains an impurity deleterious to the catalyst which comprises treating the hydrocarbon oil with a sorbent comprising a first molecular sieve zeolite having pores with an effective diameter of at least about 5 Angstroms under sorption conditions effective to remove at least some of the impurity and dewaxing the treated oil by contact under dewaxing conditions with a dewaxing catalyst comprising a second molecular sieve zeolite having pores with an effective diameter of at least about 5 Angstroms, and equal to or smaller than the effective diameter of the pores of the first molecular sieve zeolite.

The present invention provides a catalytic dewaxing process, which process comprises contacting a hydrocracked oil resulting from catalytically hydrocracking a hydrocarbon oil boiling above 343°C in the presence of hydrogen at a temperature from 260°C to 482°C, preferably from 343°C to 427°C, a pressure from 1480 kPa to 20786 kPa (200 psig to 3000 psig), preferably from 10443 kPa to 17338 kPa (1500 psig to 2500 psig), and a LHSV from 0.2 to 20, preferably from 0.5 to 5, with a catalyst comprising crystalline zeolite ZSM-23.

The present invention further provides such a process wherein the hydrocarbon oil boiling above 343°C is hydrocracked in the presence of hydrocracking catalyst under hydrocracking conditions including a temperature from 260°C to 482°C, preferably from 343°C to 427°C, a pressure from 6996 kPa to 20786 kPa (1000 psig to 3000 psig), preferably from 10443 kPa to 17338 kPa (1500 psig to 2500 psig), and a LHSV from 0.1 to about 5, preferably from 0.5 to 2. This invention also provides such a process wherein the dewaxed hydrocracked oil is hydrotreated in the presence of a hydrotreating catalyst under hydrotreating conditions including a temperature from 176°C to 371°C, preferably from 204°C to 316°C, a pressure from 6996 kPa to 20786 kPa (1000 psig to 3000 psig), preferably from 10443 kPa to 17338 kPa (1500 psig to 2500 psig) and a LHSV from 0.1 to 10, preferably from 0.2 to 3.

This invention provides an improved process for dewaxing hydrocracked oil. The essential feature of the process is the use of a dewaxing catalyst comprising zeolite ZSM-23. With this dewaxing catalyst, the yield of dewaxed oil is higher at comparable operating effort than the art methods. An additional advantage is that the viscosity index of the dewaxed oil is higher than that obtained by the art methods employing zeolites other than ZSM-23 (e.g. ZSM-5) in the dewaxing stage catalyst.

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The use of catalyst comprising zeolite ZSM-23 in the dewaxing reactor also provides other advantages over the art. One advantage is that the temperature required to achieve a desired pour point is higher than that for a standard catalyst, such as, for example, a zeolite ZSM-5 catalyst, more nearly matching the temperature required for the hydrocracking reactor. This minimizes the need for quenching of the 5 hydrocracked effluent from the hydrocracking stage of the process, resulting in substantial energy saving. As a consequence of these added advantages, embodiments of this invention in which the dewaxing step is integrated with the hydrocracking step and with a catalytic hydrotreating step provide an energy-efficient process for manufacturing a stabilized and dewaxed hydrocracked lubricating oil stock from a hydrocarbon feedstock boiling above about 343°C (650°F), such as vacuum gas oils, and resids substantially free of 10 asphaltenes. The process comprises passing the effluent from a catalytic hydrocracking process operation through a catalytic dewaxing process operation provided with a catalyst comprising zeolite ZSM-23. It further comprises passing the feed sequentially through a hydrocracking zone, a catalytic dewaxing zone provided with a dewaxing catalyst comprising zeolite ZSM-23 and a hydrotreating zone at high pressure conditions in each of these zones. The essential temperature and pressure parameters for the sequential 15 hydrocracking, dewaxing, and hydrotreating embodiments are shown in Table I.

An embodiment of the present process will now be illustrated by reference to Figure 1 of the drawings.

The feed to the hydrocracker, which may be any hydrocarbon oil boiling above about 343°C (650°F), such as a heavy neutral oil or a deasphalted residuum, is introduced via line 1 together with hydrogen via line 2 to hydrocracker section 3. Hydrocracker section 3 includes a catalytic hydrocracking zone at 20 conditions effective to convert in a single pass at least 20% of the feed to materials boiling below the initial boiling point of the feed.

The effluent from the hydrocracker 3 including excess hydrogen may be contaminated with free 25 hydrogen sulfide and, in some cases, with ammonia, since the hydrocracking step, in addition to saturating aromatic compounds, also is accompanied by desulfurization and denitrogenation. This effluent may be passed via line 4 to a high pressure gas-liquid separator (G/L Sep) 5 wherein the hydrocracked material is separated from contaminated hydrogen. The contaminated hydrogen may be passed from separator 5 via line 6 to a high pressure sorption section 7 wherein a substantial fraction of the hydrogen sulfide and of the ammonia are removed via line 8.

The hydrogen from sorption unit 7 may be passed via line 9 to a high pressure separator section 10 30 wherein it is separated from light hydrocarbons which are removed via line 11.

The hydrocracked material separated in separator section 5 is passed via line 12 to catalytic dewaxing section 13 along with makeup hydrogen introduced via line 14. It is important to note for purposes of this invention that the only hydrogen supplied to the catalytic dewaxer section 13 is fresh hydrogen having a hydrogen sulfide partial pressure of less than about 34.5 kPa (5 psia) and less than 100 ppm of ammonia.

35 The amount of hydrogen supplied via line 14 may be up to about the amount consumed in the process. Thus, all of the makeup hydrogen may be supplied via line 14. Alternatively, if it is desired to supply to the catalytic dewaxer 13 less than the makeup requirement of the system, the remainder may be supplied to the hydrocracker via line 15, or at any other point in the system.

The zeolitic dewaxing catalyst component, with or without a hydrogenation component, used in 40 dewaxing section 13 is zeolite ZSM-23. Zeolite ZSM-23 is described in U.S. Patent Nos. 4,076,842 and 4,104,151. The hydrogenation component associated with the ZSM-23 component of the dewaxing catalyst may be a metal from Group VIII of the Periodic Table of Elements or a mixture of such metals alone or in combination with a metal from Group VI of the Periodic Table of Elements or a mixture thereof. Examples of the metals from Group VIII for this purpose include platinum, palladium, iridium, ruthenium, cobalt and 45 nickel. The Group VI metals are chromium, molybdenum and tungsten.

The effluent from the catalytic dewaxer 13, including excess hydrogen, is passed via line 16 to hydrotreater unit 17. Catalytic hydrotreater 17 contains a hydrotreating catalyst in a hydrotreating zone at stabilizing conditions. Examples of hydrotreating catalysts include one or more metals from Group VIII (e.g. cobalt and nickel) and Group VI (e.g. molybdenum and tungsten) of the Period Table of Elements supported 50 by an inorganic oxide such as, for example, alumina or silica-alumina.

The effluent from the hydrotreater unit is passed via line 18 to a high pressure separation section 10 wherein it is treated to separate light hydrocarbons, which are removed together with a hydrogen bleed via line 11. Also separated is the hydrocarbon mixture comprising a stabilized and dewaxed hydrocracked lubricating oil stock, which is recovered via line 19. The hydrocarbon mixture containing the lubricating oil 55 stock is passed via line 19 to another unit for recovery of the lubricating oil stock, which other unit is not part of this invention. The makeup and recycle hydrogen separated in section 10 is passed via line 20 to compressor 21 to raise its pressure and then passed via line 2 to the hydrocracker 3.

In the preferred mode of operation of this embodiment, the pressure in line 20, which is downstream from pump 21, and the pressure in line 2, which is upstream of pump 21, do not differ by more than about 60 5272 kPa (750 psig).

The embodiment of the process of this invention shown in Figure 1 is illustrative of processing a hydrocarbon oil by the sequence of steps comprising hydrocracking, catalytic dewaxing by the present method and stabilization, in that order, with only fresh hydrogen provided to the catalytic dewaxer. It is known that hydrocracking by itself results in an unstable oil, and catalytic dewaxing in some instances also contributes to instability. By disposing the catalytic dewaxing step between the hydrocracking and 65

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stabilization step in the manner described in this embodiment, a very efficient over-all process results with the production of a stabilized and dewaxed hydrocracked lubricating oil stock.

It will be recognized by those skilled in the art that various separation steps conducted at high pressure may be advantageously incorporated in the process flow diagram of Figure 1. For example, a high pressure separation unit may be located in line 12 or line 16, for example, to remove a low molecular weight fraction of hydrocarbon not suitable for inclusion in the final lubricant base stock, thereby reducing the hydrocarbon load to subsequent sections.

The reaction conditions for the catalytic process steps herein described are summarized in Table I.

10

TABLE I

	Hydrocracking	Dewaxing	Hydrotreating
15 Pressure, broad, kPa (psig)	6996—20786 (1000—3000)	1480—20786 (200—3000)	6996—20786 (1000—3000)
Pressure, preferred, kPa (psig)	10443—17338 (1500—2500)	10443—17338 (1500—2500)	10443—17338 (1500—2500)
20 Temperature, broad, °C	260—482	260—482	176—371
Temperature, preferred, °C	343—427	343—427	204—316
LHSV,* broad	0.1—5	0.2—20	0.1—10
LHSV, preferred	0.5—2	0.5—5	0.2—3
25 H ₂ gas, l/l, broad (SCF/bbl, broad)	178—3560 (1000—20,000)	89—3560 (500—20,000)	89—3560 (500—20,000)
H ₂ gas, l/l, preferred (SCF/bbl, preferred)	356—1780 (2000—10,000)	89—534 (500—3000)	89—534 (500—3000)

30 *LHSV=liquid hourly space velocity, i.e. volumes of feed per volume of catalyst per hour.

A wide variety of hydrocracking catalysts are contemplated as suitable for use in the process of this invention. Such catalysts in general possess an acid function and a hydrogenation function, exemplified by a porous acidic oxide such as a silica alumina or silica zirconia associated with a nickel-tungsten or palladium or platinum, or cobalt-molybdenum or nickel-molybdenum component. In general, a Group VIII metal or a combination of a Group VI and a Group VIII metal, as the oxides or sulfides thereof, deposited on silica alumina or silica zirconia, may serve as hydrocracking catalyst. The hydrocracking itself may be conducted in two or more stages, with pretreatment of the raw feed as part of the first stage. Catalyst suitable for the dewaxing and hydrotreating steps have been described above.

40 The zeolite ZSM-23 dewaxing catalyst component may be incorporated with a matrix or binder component comprising a material resistant to the temperature and other process conditions.

Useful matrix materials include both synthetic and naturally occurring substances, as well as inorganic materials such as clay, silica and/or metal oxides. The latter may be either naturally occurring or in the form of gelatinous precipitates or gels including mixtures of silica and metal oxides. Naturally occurring clays which can be composited with the zeolite include those of the montmorillonite and kaolin families, which families include the sub-bentonites and the kaolins commonly known as Dixie, McNamee, Georgia and Florida clays or others in which the main mineral constituent is halloysite, kaolinite, dickite, nacrite or an auxite. Such clays can be used in the raw state as originally mined or initially subjected to calcination, acid treatment or chemical modification.

50 In addition to the foregoing materials, the zeolite ZSM-23 employed herein may be composited with a porous matrix material, such as alumina, silica-alumina, silica-magnesia, silica-zirconia, silica-thoria, silica-beryllia, silica-titania as well as ternary compositions such as silica-alumina-thoria, silica-alumina-zirconia, silica-alumina-magnesia and silica-magnesia-zirconia. The matrix can be in the form of a cogel. The relative proportions of zeolite ZSM-23 component and inorganic oxide gel matrix, on an anhydrous basis, may vary widely with the zeolite content ranging from between 1 to 99 percent by weight and more usually in the range of 5 to 80 percent by weight of the dry composite.

The above-defined hydrogenation component associated with the dewaxing catalyst may be on the zeolite component as above-noted or on the matrix component or both.

The following examples illustrate the process of the present invention.

60

Example 1

Since the effluent hydrocracked oil from the hydrocracking reactor is at a temperature of at least 371°C (700°F), a catalytic dewaxing stage downstream therefrom would desirably be operated at a temperature as close to 371°C (700°F) as possible while providing desirable lubricating oil yield and viscosity. This example

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compares the present process with that of the art, e.g. U.S. Patent Nos. 4,283,271 and 4,283,272, and further with expensive non-catalytic solvent dewaxing which provides high lube yields and viscosity index.

A hydrocracked charge stock having the following properties:

5	Gravity, °API	30.7
	Specific	0.8724
	Pour point, °C	46
	K.V. at 100°C, cs	7.29
	Sulfur, Wt.%	less than 0.06
10	Nitrogen, ppm	less than 1
	Distillation, D-2887, °C	
	0.5%	283
	1	293
	5	330
15	10	364
	30	446
	50	482
	70	505
	90	531
20	95	539
	98	552

was charged to a dewaxing reactor containing a catalyst extrudate of 65 wt.% alumina and 35 wt.% HZSM-23. The HZSM-23 zeolite was prepared as described in U.S. Patent No. 4,076,842 with pyrrolidine as the cation source in the synthesis reaction mixture. The hydrocracked oil was passed over the catalyst at 2859 kPa (400 psig), 445 l of hydrogen/l (2500 SCF of hydrogen/bbl) and an LHSV of 0.5. In Table II below, results are compared with those obtained with the standard dewaxing catalyst (U.S. Patent Nos. 4,283,271 and 4,283,272) at an LHSV of 1.0 so that the contact time based on catalyst zeolite content was identical. Table II also shows results obtained from the same hydrocracked material by solvent dewaxing conducted at -23°C (-10°F), 60/40 volume ratio MEK/toluene solvent and 3/1 volume ratio solvent/oil.

TABLE II
Dewaxing comparisons, Example 1

35		HZSM-23		Standard	Solvent
				catalyst	
	Temperature, °C	302	329	274	—
	Lube yield, wt.%	91.0	85.0	78.8	85.6
40	Lube properties				
	Gravity, °API	30.3	30.2	29.1	29.3
	Specific	0.8745	0.8751	0.8811	0.8800
	Pour point, °C	+7.2	-12.2	-9.4	-17.7
	K.V. at 40°C, cs	58.23	61.02	71.17	56.82
45	K.V. at 100°C, cs	7.90	8.04	8.59	7.72
	SUS at 38°C	301	316	370	294
	Viscosity index	100.6	97.6	89.8	98.7
	Distillation, D-2887, °C				
	0.5%	296	289	302	283
50	1	305	301	311	—
	5	343	341	346	324
	10	376	374	374	352
	50	479	479	479	473
	90	532	532	532	531
55	95	544	544	542	579
	98	557	557	554	—

From the above comparison it is observed that the temperature required for the HZSM-23 catalyst to provide a -12.2°C pour is about 38°C higher than for the standard art catalyst and closer to the temperature of the effluent from the hydrocracking reactor. Also, lubricating oil yield and viscosity index provided by the HZSM-23 catalyst is much higher than that provided by the standard art catalyst, being about the same as that provided by solvent dewaxing.

Example 2

The ZSM-23 dewaxing catalyst for this example was the same as that used in Example 1, except that it

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contained 0.5% platinum incorporated via impregnation with a platinum amine complex. The charge stock of Example 1 was processed over this catalyst at both 10443 kPa and 2859 kPa (1500 and 400 psig), the other conditions being the same as in Example 1. Results over the Pt/ZSM-23 catalyst, compared with results under comparable conditions over the standard dewaxing catalyst of Example 1 and solvent dewaxing are shown in Figures 2, 3 and 4. Figure 2 shows the higher average catalyst temperature attainable for the Pt/ZSM-23 catalyst compared to that attainable for the standard catalyst at like product pour point. Figure 3 shows the higher lubricating oil yield attainable by the Pt/ZSM-23 catalyst compared to that attainable by the standard catalyst and even solvent dewaxing at like product pour point. Figure 4 shows the higher viscosity index attainable by the Pt/ZSM-23 catalyst compared to that attainable by the standard catalyst at like product pour point.

Example 3

The charge stock to the dewaxing reactor in this example was a hydrocracked oil having the following properties:

15	Gravity, °API	33.1
	Specific	0.8597
	Pour point, °C	29.4
20	K.V. at 100°C, cs	4.25
	Sulfur, wt.%	0.02
	Nitrogen, ppm	less than 0.2
	Distillation, D-2887, °C	
25	0.5%	282
	1	291
	5	321
	10	344
	30	389
	50	415
	70	436
30	90	466
	95	479
	98	493

Results of catalytically dewaxing this hydrocrackate over the Pt/ZSM-23 catalyst and the standard catalyst used in U.S. Patent Nos. 4,283,271 and 4,283,272 at 10443 kPa and 2859 kPa (1500 psig and 400 psig), respectively, are summarized in Table III. The other conditions for this example are the same as those for Examples 1 and 2.

TABLE III
Dewaxing comparisons, example 3

		Pt/ZSM-23	Standard catalyst
45	Pressure, kPa (psig)	10443 1500	2859 400
	Temperature, °C	316	275
	Lube yield, wt.%	79.5	76.8
50	Lube properties		
	Gravity, °API	32.6	31.3
	Specific	0.8623	0.8692
	Pour point, °C	-29	-29
	K.V. at 40°C, cs	28.82	28.20
	K.V. at 100°C, cs	4.99	4.82
55	SUS at 38°C	149.1	146.2
	Viscosity index	96.4	86.1
	Distillation, D-2887, °C		
60	0.5%	319	288
	1	327	296
	5	352	324
	10	368	344
	50	422	415
	90	474	472
	95	477	489
65	98	510	531

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The above results show that even with this charge stock the ZSM-23 catalyst again requires a higher temperature than the standard catalyst and provides a higher product yield of higher viscosity index than the standard catalyst.

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Claims

1. A catalytic dewaxing process, which process comprises contacting a hydrocracked oil resulting from catalytically hydrocracking a hydrocarbon oil boiling above 343°C in the presence of hydrogen at a temperature from 260°C to 482°C, a pressure from 1480 kPa to 20786 kPa (200 psig to 3000 psig) and a LHSV from 0.2 to 20 with a dewaxing catalyst comprising crystalline zeolite ZSM-23.
2. A process according to claim 1 wherein the hydrocarbon oil boiling above 343°C is hydrocracked in the presence of a hydrocracking catalyst under hydrocracking conditions including a temperature from 260°C to 482°C, a pressure from 6996 kPa to 20786 kPa (1000 psig to 3000 psig) and a LHSV from 0.1 to 5.
3. A process according to claim 1 or 2 wherein the dewaxed hydrocracked oil is hydrotreated in the presence of a hydrotreating catalyst under hydrotreating conditions including a temperature from 176°C to 371°C, a pressure from 6996 kPa to 20786 kPa (1000 psig to 3000 psig) and a LHSV from 0.1 to 10.
4. A process according to any preceding claim wherein the dewaxing or the hydrocracking catalyst has associated therewith a hydrogenation component.
5. A process according to claim 4 wherein the hydrogenation component is one or more Group VIII metals optionally in admixture with one or more metals from Group VI of the Periodic Table of Elements.
6. a process according to claim 4 or 5 wherein the catalyst further comprises a binder material.
7. a process according to claim 6 wherein the binder material comprises alumina.
8. a process according to any preceding claim wherein the dewaxing conditions include a temperature from 343°C to 427°C, a pressure from 10443 kPa to 17338 kPa (1500 psig to 2500 psig) and a LHSV from 0.5 to 5.
9. A process according to any preceding claim wherein the hydrocracking conditions include a temperature from 343°C to 427°C, a pressure from 10443 kPa to 17338 kPa (1500 psig to 2500 psig) and a LHSV from 0.5 to 2.
10. A process according to any preceding claim wherein the hydrotreating conditions include a temperature from 204°C to 316°C, a pressure from 10443 kPa to 17338 kPa (1500 psig to 2500 psig) and a LHSV from 0.2 to 3.

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Patentansprüche

1. Katalytisches Entparaffinierungsverfahren, welches den kontakt eines hydrogecrackten Öls, daß aus dem katalytischen hydrocracken eines oberhalb 343°C siedenden bohlenwasserstofföls resultiert, in Gegenwart von Wasserstoff bei einer Temperatur von 260 bis 482°C, einem Druck von 1480 kPa bis 20786 kPa (200 bis 3000 psig) und eine LHSV von 0,2 bis 20 mit einem Entparaffinierungskatalysator umfaßt, der einen kristallinen Zeolith ZSM-23 umfaßt.
2. Verfahren nach Anspruch 1, worin das oberhalb 343°C siedende Kohlenwasserstofföl in Gegenwart eines Hydrocrackkatalysators unter Hydrocrackbedingungen hydrogecrackt wird, die eine Temperatur von 260°C bis 482°C, einen Druck von 6996 kPa bis 20786 kPa (1000 psig bis 3000 psig) und eine LHSV von 0,1 bis 5 einschließen.
3. Verfahren nach Anspruch 1 oder 2, worin das entparaffinierte hydrogecrackte Öl in Gegenwart eines Hydrobehandlungskatalysators unter Hydrobehandlungsbedingungen hydrobehandelt wird, die eine Temperatur von 176°C bis 371°C, einen Druck von 6996 kPa bis 20786 kPa (1000 bis 3000 psig) und eine LHSV von 0,1 bis 10 umfassen.
4. Verfahren nach einem der vorstehenden Ansprüche, worin der Entparaffinierungs- oder Hydrocrackkatalysator eine damit verbundene Hydrierungskomponente aufweist.
5. Verfahren nach Anspruch 4, worin die Hydrierungskomponente ein oder mehrere Metalle der Gruppe VIII, wahlweise in Vermischung mit ein oder mehreren Metallen aus der Gruppe VI des Periodensystems der Elemente darstellt.
6. Verfahren nach Anspruch 4 oder 5, worin dieser Katalysator weiterhin ein Bindematerial umfaßt.
7. Verfahren nach Anspruch 6, worin das Bindematerial Aluminiumoxid darstellt.
8. Verfahren nach einem der vorstehenden Ansprüche, worin die Entparaffinierungsbedingungen eine Temperatur von 343 bis 427°C, einen Druck von 10443 KPa bis 17338 kPa (1500 psig bis 2500 psig) und eine LHSV von 0,5 bis 5 umfassen.
9. Verfahren nach einem der vorstehenden Ansprüche, worin die Hydrocrackbedingungen eine Temperatur von 343 bis 427°C, einen Druck von 10443 bis 17338 kPa (1500 bis 2500 psig) und eine LHSV von 0,5 bis 2 umfassen.
10. Verfahren nach einem der vorstehenden Ansprüche, worin die Hydrobehandlungsbedingungen eine Temperatur von 204 bis 316°C, einen Druck von 10443 bis 17338 kPa (1500 bis 2500 psig) und eine LHSV von 0,2 bis 3 umfassen.

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Revendications

1. Un procédé de déparaffinage catalytique, ce procédé consistant à mettre un catalyseur de déparaffinage consistant en une zéolite ZSM-23 cristalline au contact d'une huile hydrocraquée résultant d'un hydrocraquage catalytique d'une huile hydrocarbonée dont le point d'ébullition est supérieur à 343°C en présence d'hydrogène, à une température comprise entre 260°C et 482°C, sous une pression comprise entre 1 480 kPa et 20 786 kPa (200 psig et 3 000 psig) et une vitesse spatiale horaire liquide comprise entre 0,2 et 20.
2. Un procédé selon la revendication 1, dans lequel l'huile hydrocarbonée dont la température d'ébullition est supérieure à 343°C est hydrocraquée en présence d'un catalyseur d'hydrocraquage, dans des conditions d'hydrocraquage incluant une température comprise entre 260°C et 482°, une pression comprise entre 6 996 kPa et 20 786 kPa (1 000 psig et 3 000 psig) et une vitesse spatiale horaire liquide comprise entre 0,1 et 5.
3. Un procédé selon la revendication 1 ou 2, dans lequel l'huile hydrocraquée déparaffinée est hydrotraitée en présence d'un catalyseur d'hydrotraitement, dans des conditions d'hydrotraitement incluant une température comprise entre 176°C et 371°C, une pression comprise entre 6 996 kPa et 20 786 kPa (1 000 psig et 3 000 psig) et une vitesse spatiale horaire liquide comprise entre 0,1 et 10.
4. Un procédé selon l'une quelconque des revendications précédentes, dans lequel le catalyseur d'hydrocraquage ou de déparaffinage est associé à un constituant d'hydrogénéation.
5. Un procédé selon la revendication 4, dans lequel le constituant d'hydrogénéation est un ou plusieurs métaux du groupe VIII, éventuellement associés à un ou plusieurs métaux du groupe VI, de la Classification Périodique des Éléments.
6. Un procédé selon la revendication 4 ou 5, dans lequel le catalyseur comprend en outre un matériau formant liant.
7. Un procédé selon la revendication 6, dans lequel le matériau formant liant comprend de l'alumine.
8. Un procédé selon l'une quelconque des revendications précédentes, dans lequel les conditions de déparaffinage incluent une température comprise entre 343°C et 427°C, une pression comprise entre 10 443 kPa et 17 338 kPa (1 500 psig et 2 500 psig) et une vitesse spatiale horaire liquide comprise entre 0,5 et 5.
9. Un procédé selon l'une quelconque des revendications précédentes, dans lequel les conditions d'hydrocraquage incluent une température comprise entre 343°C et 427°C, une pression comprise entre 10 443 kPa et 17 338 kPa (1 500 psig et 2 500 psig) et une vitesse spatiale horaire liquide comprise entre 0,5 et 2.
10. Un Procédé selon l'une quelconque des revendications précédentes, dans lequel les conditions d'hydrogénéation incluent une température comprise entre 204°C et 316°C, une pression comprise entre 10 443 kPa et 17 338 kPa (1 500 psig et 2 500 psig) et une vitesse spatiale horaire liquide comprise entre 0,2 et 3.

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FIG. I
PROCESS FLOW DIAGRAM

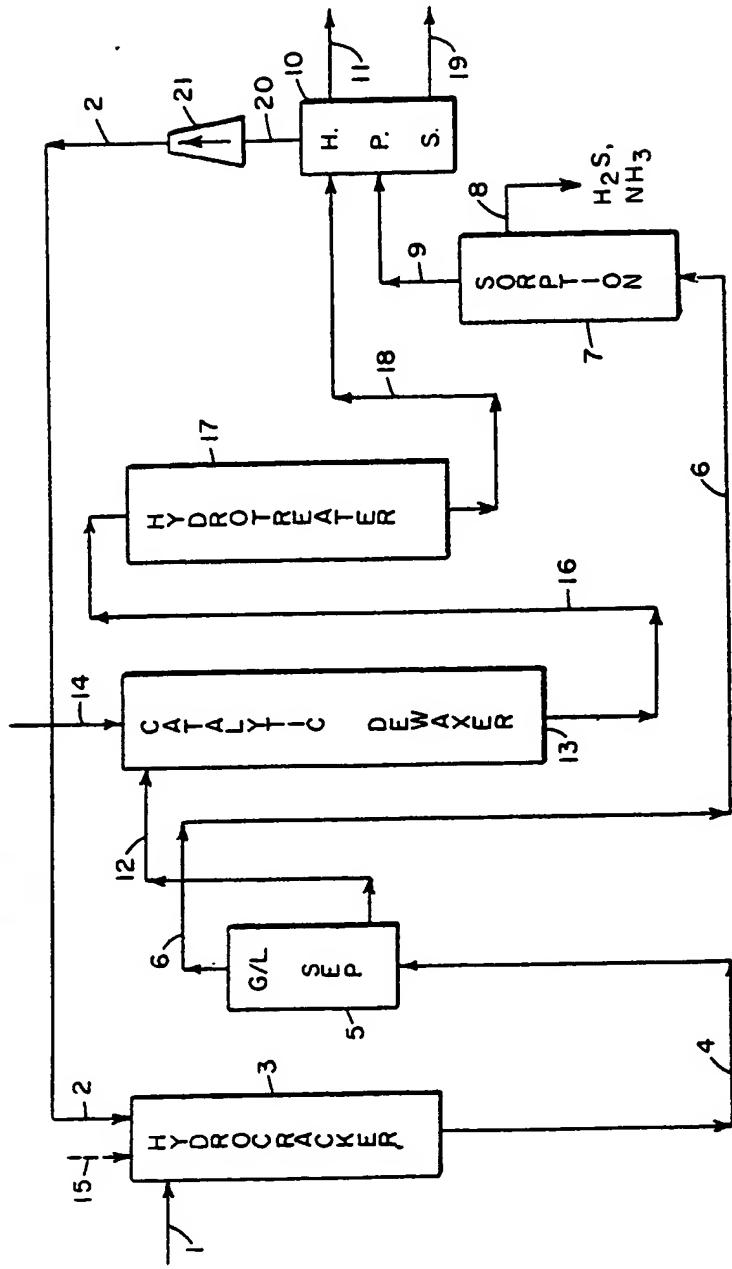


FIG. 2

CATALYST TEMPERATURE
V.
PRODUCT POUR POINT

- PT/ZSM-23 CATALYST, 1500 PSIG
- PT/ZSM-23 CATALYST, 400 PSIG
- STANDARD CATALYST, 400 PSIG

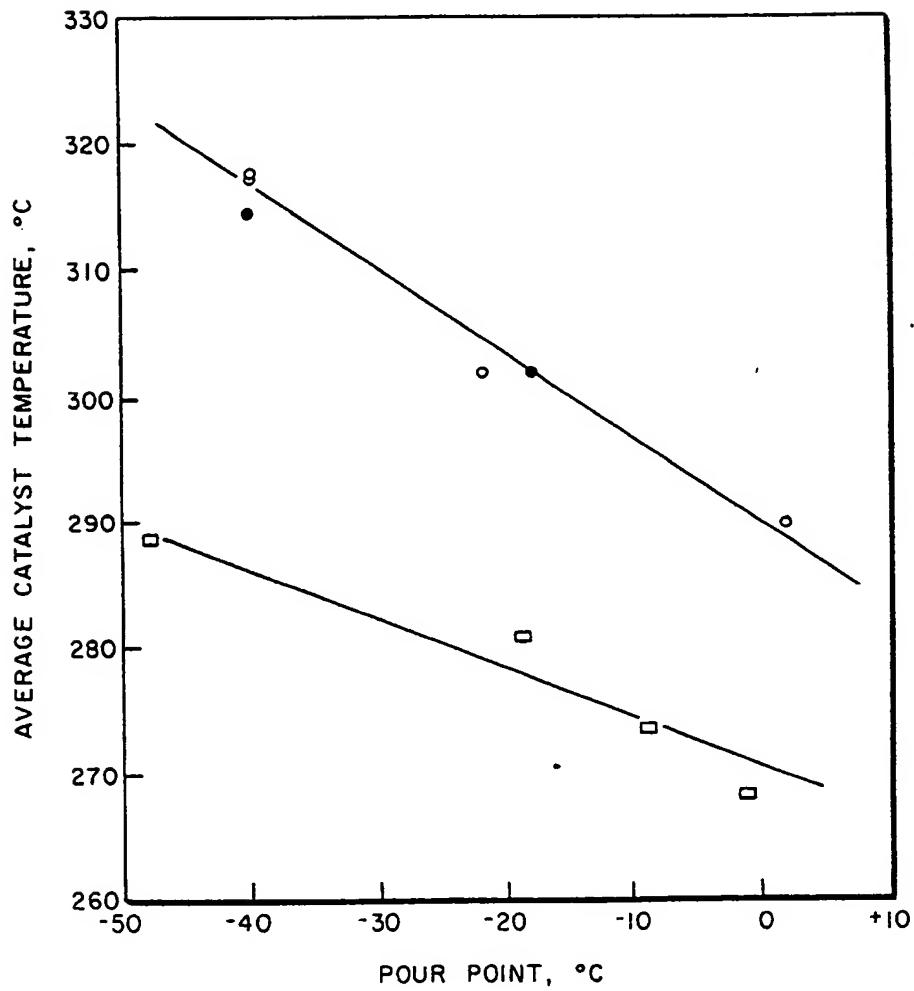
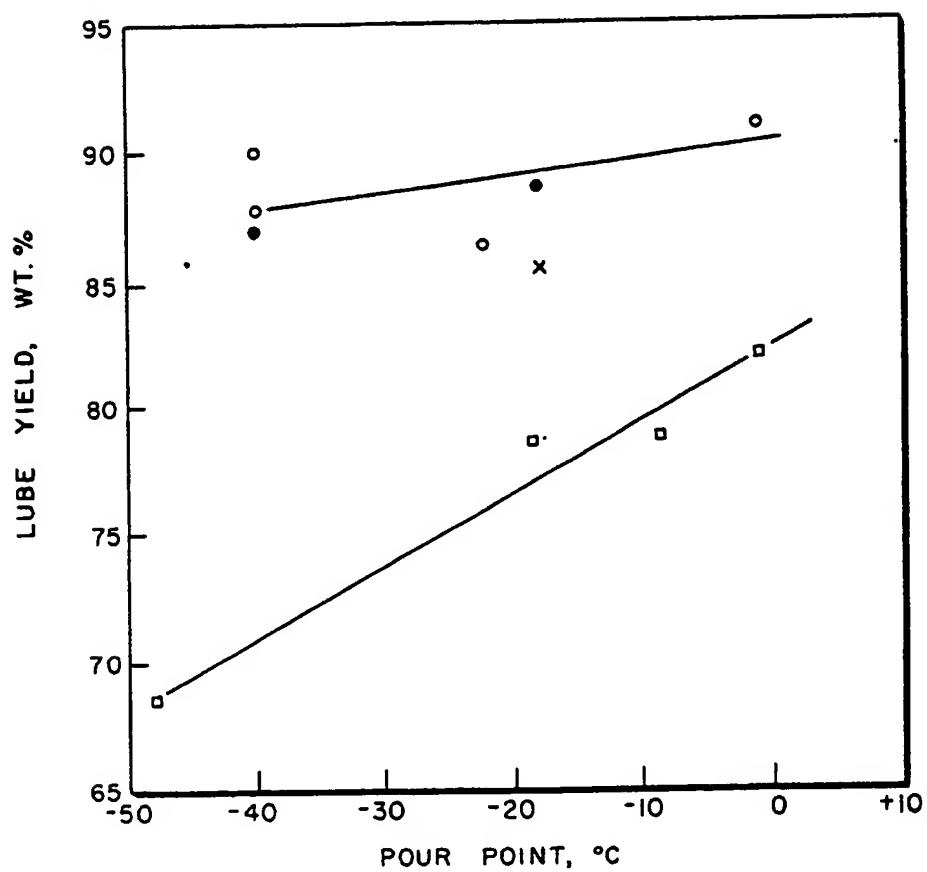


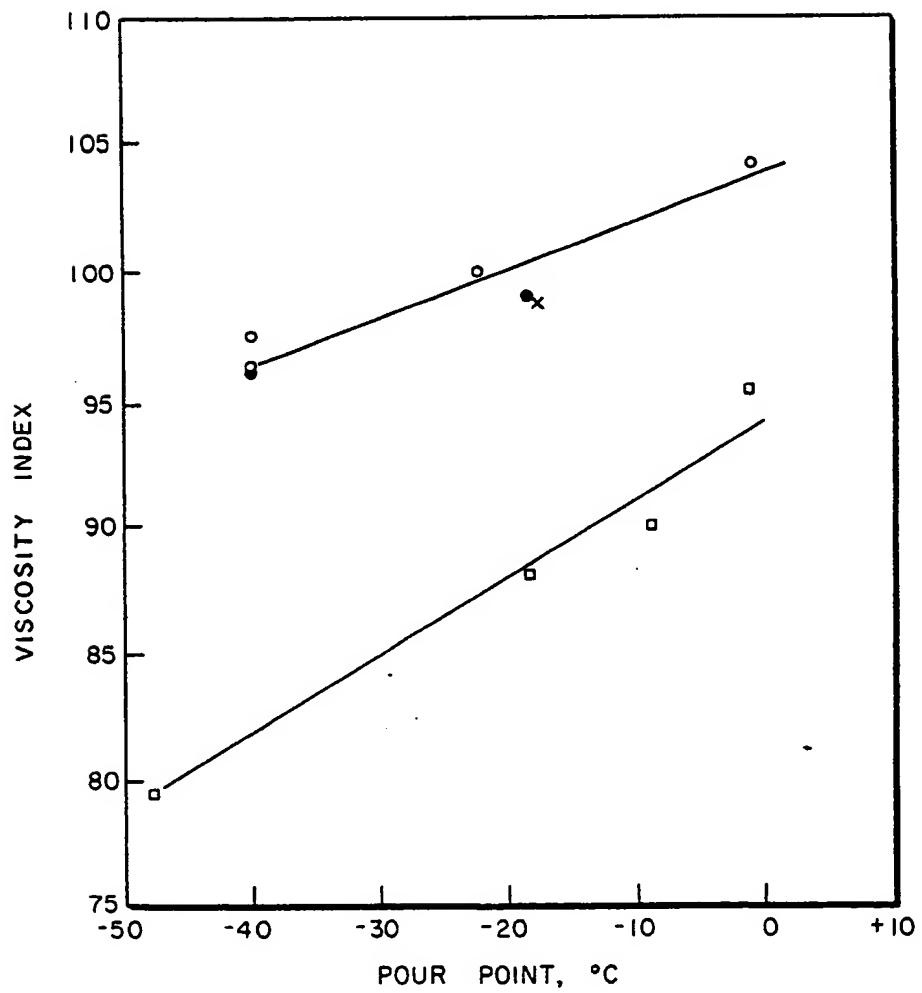
FIG. 3 LUBE YIELD V. POUR POINT

- PT/ZSM-23 CATALYST, 1500 PSIG
- PT/ZSM-23 CATALYST, 400 PSIG
- STANDARD CATALYST, 400 PSIG
- × SOLVENT DEWAXING



VISCOSITY INDEX V. POUR POINT
FIG. 4

- PT/ZSM-23 CATALYST, 1500 PSIG
- PT/ZSM-23 CATALYST, 400 PSIG
- STANDARD CATALYST, 400 PSIG
- × SOLVENT DEWAXING



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